Huludao Zinc Refinery Effluent Treatment Plant

JOINT VENTURE Of MITSUI MINING & SMELTING CO.,LTD MITSUBISHI MATERIAL CORPORATION

Process Technology and Plant Engineering by MESCO Inc.

Location of Effluent Treatment Plant (Huludao Zinc Refinery)



Main elements of the Effluent

1999 Survey

| | Flow | H_2SO_4 | Zn | Сd |
|-------------------------------|-----------|-----------|---------|---------|
| | (m^3/d) | (m g/l) | (m g/l) | (m g/l) |
| Effluentfrom Zinc refinery | 600 | 20000 | 1600 | 400 |
| Effluent from Copper refinery | 600 | 20000 | 4800 | 1200 |

| Рb | As | F | Сu | Нg |
|---------|---------|---------|---------|---------|
| (m g/l) |
| 420 | 1460 | 1700 | 1.6 | 10.0 |
| 110 | 8400 | 1600 | 167 | 0.8 |
| 270 | 4930 | 1650 | 84.3 | 9.0 |

Treatment methods of materials

| H_2SO_4 | : Removal method of calcium sulfate $(CaSO_4 \cdot 2H_2O)$ |
|-------------|---|
| Zn、Cd、Pb、Cu | Flocculation Sedimentation Method with insoluble salt Ion exchange process Magnetic separation with ferrite |
| As F | Coprecipitation method Flocculation Sedimentation Method with sulfide Calcium fluoride method |
| Hg | Flocculation Sedimentation Method with sulfide Absorption Method |

The process of our Effluent Plant

(Specializing and combining the disposing method of various heavy metals respectively)

1st Neutralization Treatment

*Removing SO₄

2nd Neutralization Treatment

*Removing various heavy metals using the Method by

Flocculation Sedimentation with insoluble salt

3rd Final Treatment

*Removing heavy metals which not enough to be removed by 2nd neutralization treatment by using the method of Flocculation Sedimentation with sulfide

Sand Filtration Treatment

* Removing suspended solids remained after Solid-liquid separator

First Neutralization Treatment (Precipitation method of Calcium sulfate)

<Processing Object> SO4²⁻

<Treating Method>

To neutralize with hydrated lime (Ca(OH)₂) upto approximately pH 2.5.

<Reaction>

Calcium sulfate (CaSO₄•2H₂O) is produced reacting SO₄²⁻ and Ca²⁺ Ca(OH)₂ + H₂SO₄ \rightarrow CaSO₄•2H₂O \downarrow





2nd Neutralization Treatment

< Treatment Materials >

Zn, Cd, Pb, Cu, As, F(Fe)

< Treatment Method >

*To add FeSO4 \cdot 7H₂O to the Effluent to remove Arsenic with precipitation method.

*To neutralize the Effluent with hydrated lime (Ca(OH)₂) upto pH 11 approximately.

*To prompote the oxidation of Fe(OH)₂.

< Reaction >

 $\begin{array}{rcl} \mathrm{M}^{2+} & + & \mathrm{Ca}(\mathrm{OH})_2 \rightarrow & \mathrm{M}(\mathrm{OH})_2 \downarrow & + & \mathrm{Ca}^{2+} \\ \mathrm{Fe}^{2+} & + & \mathrm{Ca}(\mathrm{OH})_2 \rightarrow & \mathrm{Fe}(\mathrm{OH})_2 \downarrow & + & \mathrm{Ca}^{2+} \\ \mathrm{Fe}(\mathrm{OH})_2 & + & 1/4\mathrm{O}_2 & + & 1/2\mathrm{H}_2\mathrm{O} \rightarrow & \mathrm{Fe}(\mathrm{OH})_3 \downarrow \\ \mathrm{2F}^- & + & \mathrm{Ca}(\mathrm{OH})_2 \rightarrow & \mathrm{CaF}_2 \downarrow & + & 2\mathrm{OH}^- \end{array}$



2nd Neutralization Treatment



3rd Treatment

< Treatment Materials > As, Hg

< Treatment Method >

* After neutralization of secondary effluent with H₂SO₄ upto pH 5-6 approximately, Na₂S to be added.
* To add FeSO₄, 7H₂O and flocculent to collect sludge.
* To re-neutralize with NaOH upto pH 8.

< Reaction >

*To form insoluble As_2S_3 , HgS reacting of As and Hg with S $2H_3AsO_3 + 3Na_2S \rightarrow As_2S_3 + 6NaOH$ $Hg^+ + Na_2S \rightarrow HgS + 2Na^+$



Sand filtration treatment

Flowchart of plant (First and second neutralization treatment)



Flowchart of plant (Third treatment and Sand filtration treatment)



Cross-section diagram of pilot plant



Planform of pilot plant



Centrifuge



Filterpress



Operation management of tratment plant



- * Monitoring system
- Function management of equipments

 Start, Stop, state of trouble
 Indication of instantaneous value of pH
 Indication of treating water quantity
 State of each progression
- •Output of monthly and daily report Maximum, minimum, and average of pH and Quantities of treatment water
- * Monitoring system
- •Camera
 - Filter press
 - Centrifuge
- Paging system Filter press Centrifuge Reagent room

Control System of Treatment plant



Main Control room

- * Main control panel
 - Automatic controll
 - Select of operating condition of each equipment (Automatic, Manual, and Stop)
 - Set the level of pH
 - Indication of quantities of treating water
 - Indication of several alerm
- * Local control panel
 - Manual operation
 - Maintenance of equipments

Target treatment water and Actual treated water

< Properties of Inlet Water >

| | рН | Zn | Cd | Pb | As | F | Cu | Hg |
|----------------|------|--------|--------|--------|--------|--------|--------|--------|
| | | (mg/l) |
| Target | 0.4 | 3200 | 800 | 270 | 4930 | 1650 | 84.3 | 9.0 |
| Actual Max. | 0.44 | 4343 | 379 | 153 | 1037 | 548 | 343 | 1.1 |
| Actual Average | 1.8 | 269 | 38 | 121 | 44 | 35 | 2.6 | 4.0 |

< Properties of Treated Water >

| | рН | Zn (mg/l) | Cd (mg/l) | Pb (mg/l) | As (mg/l) | F (mg/l) | Cu (mg/l) | Hg (mg/l) | SS (mg/l) |
|--------|---------|--------------|--------------|--------------|--------------|-------------|---------------|-----------------|--------------|
| Target | 6~9 | 4.0 | 0.1 | 1.0 | 0.5 | 15 | 1.0 | 0.1 | 150.0 |
| Actual | 6.9-8.5 | 0.5-2.0 | 0.05-0.15 | 0.5-2.0 | 0.2-0.4 | 10-15 | 0.08- 0.15 | 0.003- 0.008 | 30-72 |

< Quantities of Treatment Water>

| | (m3/Day) |
|--------|----------|
| Target | 1200 |
| Actual | 500-1080 |

Target and Actual Sludge

< Sediments >

Gypsum : Target :39.7t-Dry/d (45.2t-Wet/d) Moisture content 12%

Actual :1.5t-Dry/d (1.7t-Wet/d) Average amount Moisture content 12% Actual performance

Sludge :

- Target:37.1t-Dry/d(106.1t-Wet/d)Moisture content 65%
- Acutual: 4 t-Dry/d (11.4t-Wet/d) Average amount Moisture content 60% Actual performance

Target and Actual Sludge < Crystal picture of Gypsum>



Good Crystal Figure

